Simulations of Cyclic Voltammetry for Electric Double Layers in Asymmetric Electrolytes: A Generalized Modified Poisson–Nernst–Planck Model

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Supporting Information

ABSTRACT: This paper presents a generalized modified Poisson–Nernst–Planck (MPNP) model derived from first principles based on excess chemical potential and Langmuir activity coefficient to simulate electric double-layer dynamics in asymmetric electrolytes. The model accounts simultaneously for (1) asymmetric electrolytes with (2) multiple ion species, (3) finite ion sizes, and (4) Stern and diffuse layers along with Ohmic potential drop in the electrode. It was used to simulate cyclic voltammetry (CV) measurements for binary asymmetric electrolytes. The results demonstrated that the current density increased significantly with decreasing ion diameter and/or increasing valency $|z_i|$ of either ion species. By contrast, the ion diffusion coefficients affected the CV curves and capacitance



only at large scan rates. Dimensional analysis was also performed, and 11 dimensionless numbers were identified to govern the CV measurements of the electric double layer in binary asymmetric electrolytes between two identical planar electrodes of finite thickness. A self-similar behavior was identified for the electric double-layer integral capacitance estimated from CV measurement simulations. Two regimes were identified by comparing the half cycle period τ_{CV} and the "RC time scale" τ_{RC} corresponding to the characteristic time of ions' electrodiffusion. For $\tau_{RC} \ll \tau_{CV}$, quasi-equilibrium conditions prevailed and the capacitance was diffusion-independent while for $\tau_{RC} \gg \tau_{CV}$, the capacitance was diffusion-limited. The effect of the electrode was captured by the dimensionless electrode electrical conductivity representing the ratio of characteristic times associated with charge transport in the electrolyte and that in the electrode. The model developed here will be useful for simulating and designing various practical electrochemical, colloidal, and biological systems for a wide range of applications.

1. INTRODUCTION

Cyclic voltammetry (CV) is a powerful technique in the field of electrochemistry.^{1–3} It has been the subject of intense studies in electrochemical sensing^{1–3} and in electrical energy storage and conversion.^{4–9} In these applications,^{4–9} the electric potential is typically above 1 V, while the electrolyte concentration is at least 1 mol/L. Numerous studies^{9–23} have demonstrated that the finite ion size must be accounted for when simulating electric double layers at such large electric potential and/or large electrolyte concentrations. However, these studies have been mostly limited to binary and symmetric electrolytes.^{9–23} Practical electrolytes are typically asymmetric in nature due to the difference in (i) their ion diffusion coefficients,²⁴ (ii) their ion valencies such as aqueous H₂SO₄ and Na₂SO₄. Moreover, the use of electrolyte mixtures with more than two ion species have been investigated in many practical applications such as supercapacitors,^{26–28} water desalination,^{29,30} electrokinetics in colloidal systems,^{31–40} electrochemical measurements involving supporting electrolytes,^{41–43} and various biological processes including gating and permeation in ion channels.^{44–50}

Existing simulations of asymmetric electrolytes based on continuum theory and accounting for finite ion size are mainly limited to equilibrium conditions.^{21,31–40,51–62} For example, Bikerman⁶³ developed the first equilibrium modified Poisson– Boltzmann (MPB) model accounting for finite ion size. This model applies to electrolytes with anions and cations having different volumes but symmetric valency. Borukhov et al.^{51,52} and Silalahi et al.⁵³ developed MPB models valid for binary electrolytes with asymmetric valency but identical ion diameters. Their model was later extended to binary asymmetric electrolytes with unequal ion diameters.^{54,55} Biesheuvel and coworkers^{56–58} and Alijó et al.⁴⁰ developed more general MPB models valid for asymmetric electrolytes and/or multiple ion species with different ion sizes and valencies. This was accomplished by incorporating an excess chemical potential term based on the Boublik–Mansoori–Carnahan–Starling–Leland equation-of-state. It directly relates the excess chemical

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potential to the local ion concentrations, ions' effective diameters, and their exclusion volumes.^{40,56–58} Moreover, Tresset⁵⁹ developed a generalized Poisson–Fermi model for asymmetric electrolytes and multiple ion species based on the lattice gas approach by considering ions in discrete cells of different volumes. In addition, Li and co-workers^{60–62} developed a model for asymmetric electrolytes based on the variational principle while accounting for the finite sizes of both ions and solvent molecules. Alternatively, Horno and co-workers^{31–37} developed a MPB model for asymmetric electrolytes by directly applying a "Langmuir-type" correction to the equilibrium ion concentration given by the Boltzmann distribution.

Figure 1a shows a schematic of the electric double layer structure consisting of Stern and diffuse layers forming near a



Figure 1. Schematic and the computational domain of the electric double layer structure consisting of Stern and diffuse layers (a) near a planar electrode (i.e., with the half domain) and (b) between two planar electrodes (i.e., with the full domain). Here, the ion diameters of large and small ion species are denoted by a_1 and a_2 , respectively.

planar electrode.^{1,9,64} Several studies have considered ion species with different effective diameters resulting in multiple Stern layers with different thicknesses near the electrode surface.^{36–40} There were no free charges within the Stern layer immediately adjacent to the electrode surface while all ion species coexisted in the diffuse layer.^{36–40} By contrast, only ion species of intermediate sizes existed in the intermediate Stern layer(s). Such electric double layer structure was typically used along with PB or MPB models.^{36–40} However, the associated ion concentrations do not satisfy the overall electroneutrality condition across the electrolyte domain expressed as $\sum_{i=1}^{N} \int_{-L}^{L} z_i c_i(x,t) = 0$, even for uniform concentrations typically used as initial conditions.^{9,17–23} This was caused by the small

ions present in the intermediate Stern layer(s). For example, for binary and asymmetric electrolytes with valencies $(z_i)_{1 \le i \le 2}$ and initial bulk ion concentrations $(c_{i\infty})_{1 \le i \le 2}$, the above integral initially reduces to $\sum_{i=1}^{2} \int_{-L}^{L} z_i c_{i\infty} \, dx = 2z_2 c_{2\infty} (H_1 - H_2) \neq 0$ where $H_i = a_i/2$ (i = 1 and 2) is the Stern layer boundaries defined according to the diameters of the larger (a_1) and smaller (a_2) ions, respectively. Note that $c_1(x,t)$ and $c_2(x,t)$ were nonzero for $-L + H_1 \le x \le L - H_1$ and $-L + H_2 \le x \le L - H_2$, respectively. This issue becomes particularly severe when simulating electric double layers in a finite electrolyte domain.

This paper aims to develop a model, from first principles, for simulating electric double-layer dynamics valid for asymmetric electrolytes and/or for multiple ion species accounting for different ion diameters, as well as different valencies and diffusion coefficients. The model was used to simulate CV measurements for binary asymmetric electrolytes.

2. BACKGROUND

2.1. Cyclic Voltammetry. In CV measurements, the surface potential ψ_s is imposed to vary periodically and linearly with time *t* as

$$\psi_{s}(t) = \begin{cases}
\psi_{\max} - v[t - 2(m - 1)\tau_{CV}] & (1a) \\
\text{for } 2(m - 1)\tau_{CV} \le t < (2m - 1)\tau_{CV} \\
\psi_{\min} + v[t - (2m - 1)\tau_{CV}] & (1b) \\
\text{for } (2m - 1)\tau_{CV} \le t < 2m\tau_{CV}
\end{cases}$$

where v is the scan rate in V/s, m(= 1, 2, 3,...) is the cycle number, and $\tau_{\rm CV} = (\psi_{\rm max} - \psi_{\rm min})/v$ is half the cycle period. The latter represents the time for varying the surface potential from its maximum $\psi_{\rm max}$ to its minimum $\psi_{\rm min}$ values or versa vice. Here, $\psi_{\rm max} - \psi_{\rm min}$ is referred to as the "potential window". Note that the measurements are referred to as "linear sweep voltammetry" when $\psi_{\rm s}(t) = \psi_{\rm min} + vt$ or $\psi_{\rm s}(t) = \psi_{\rm max} - vt$.

The surface charge density q_s accumulated at the electrode surface during one cycle can be estimated by computing the area enclosed by the CV curves.⁹ Then, the areal integral capacitance C_s (in F/m²) can be computed from CV measurements as⁹

$$C_{\rm s} = \frac{q_{\rm s}}{\psi_{\rm max} - \psi_{\rm min}} = \frac{1}{\psi_{\rm max} - \psi_{\rm min}} \oint \frac{j_{\rm s}}{2\nu} \, \mathrm{d}\psi_{\rm s} \tag{2}$$

where j_s is the surface current density (in A/m²).

2.2. Modeling of Electric Double Layer Dynamics. Recent efforts have been made to account for the effect of finite ion size in modeling ion transport in concentrated electrolyte solutions and/or under large electric potential.^{18–23,44–50,65–67} For example, Kilic et al.¹⁹ derived a modified Poisson–Nernst–Planck (MPNP) model valid for binary and symmetric electrolytes under large electrolyte concentration and electric potential. The authors added an excess term accounting for the entropic contribution due to finite-size ions in the expression of the Helmholtz free energy. This resulted in an excess term in the expressions of the chemical potentials and mass fluxes.^{19–22} However, this MPNP model does not apply to asymmetric electrolytes or to multiple ion species.^{9,17–23} Alternatively, several authors^{65–67} incorporated the finite ion

Alternatively, several authors^{65–67} incorporated the finite ion size in ion mass fluxes using the activity coefficient to account for the deviation from ideal electrolyte solutions. However, these studies^{65–67} were also limited to binary and symmetric

electrolytes. Note that the MPNP model developed by Kilic et al.¹⁹ can be also formulated in a form equivalent to that based on the activity coefficient.^{21,22,37} Based on this MPNP model,¹⁹ Wang and Pilon⁹ performed numerical simulations reproducing CV measurements for electric double layer capacitors with binary and symmetric electrolytes for large concentration and potential window. The model simultaneously accounted for the finite ion size, Stern and diffuse layers, and the electrode electrical conductivity. A scaling analysis was performed, and dimensionless numbers governing CV measurements were identified.⁹

Davidson and Goulbourne⁴⁴ extended the MPNP model to multiple ion species but with symmetric ion diameter and valency. Eisenberg and co-workers^{45–47} developed a MPNP model for binary asymmetric electrolytes based on the variation principle. Horng et al.⁴⁸ later extended this model^{45–47} for asymmetric electrolytes with multiple ion species. However, these MPNP models^{45–48} were expressed as integral-differential equations, thus making the numerical solution procedure highly involved particularly for three-dimensional geometries.

Lu and Zhou^{49,50} extended the expression of chemical potential developed in refs.^{51,52} and proposed a "size-modified" Poisson–Nernst–Planck (SMPNP) model for asymmetric electrolytes and multiple ion species. In their model,^{49,50} they introduced a parameter " $k_i = a_i/a_0$ " representing the ratio of ion diameter a_i and the diameter of solvent molecules a_0 . The authors considered different cases for $k_i > 1$ and justified that the model successfully constrained the ion concentrations below their maximum values. However, this SMPNP model breaks down when neglecting the size of solvent molecules and as $k_i \rightarrow \infty$ the excess term accounting for finite ion sizes approaches infinity.

To the best of our knowledge, no study has simulated CV curves for electric double layer capacitors with asymmetric electrolytes and/or with multiple ion species while accounting for the finite ion size. This paper aims to develop, from first principles, a model for simulating electric double-layer dynamics valid for asymmetric electrolytes and/or for multiple ion species. It simultaneously accounts for (1) asymmetric electrolytes with (2) multiple ion species of (3) finite ion size, and for (4) Stern and diffuse layers. The model will be useful for simulating electric double layers in various electrochemical, colloidal, and biological systems.

3. ANALYSIS

3.1. Generalized Modified Poisson–Nernst–Planck Model. Previous studies^{21,22,65–69} established that the effect of finite ion size on the electric double layer dynamics can be generally accounted for by employing the activity coefficient γ_i in the expression of the chemical potential of each ion species "*i*". The ion mass flux is proportional to the gradient of chemical potential. Then, a generalized modified Poisson– Nernst–Planck (GMPNP) model consisting of Gauss law coupled with the mass conservation equations for each one of the *N* ion species can be formulated as

$$\begin{cases} \nabla \cdot (\varepsilon_0 \varepsilon_r \nabla \psi) = -F \sum_{i=1}^N z_i c_i & (3a) \\ \frac{\partial c_i}{\partial t} = \nabla \cdot \left[D_i c_i \left(\frac{F z_i}{R_u T} \nabla \psi + \nabla \ln(\gamma_i c_i) \right) \right] & (3b) \\ \text{for } i = 1, 2, ..., N \end{cases}$$

where ψ is the local electric potential, while c_i and D_i are the molar concentration and diffusion coefficient of ion species "*i*" in the electrolyte solution, respectively. Here, ε_0 and ε_r are the free space permittivity ($\varepsilon_0 = 8.854 \times 10^{-12} \text{ F/m}$) and the relative permittivity of the electrolyte solution, respectively. The temperature is denoted by T (in K), while F and R_u are the Faraday constant (F = 96485.3 sA/mol) and the universal gas constant ($R_u = 8.314 \text{ JK}^{-1} \text{ mol}^{-1}$), respectively.

Among various forms of activity coefficient existing in the literature, the "Langmuir type" activity coefficient^{31–37,65,70–73} directly relates γ_i to the ion diameter a_i to account for the exclusion volume caused by the finite size of ion species. It is expressed as^{70,71}

$$\gamma_{i} = \frac{1}{1 - \sum_{i=1}^{N} \frac{c_{i}}{c_{i,\max}}}$$
(4)

where $c_{i,\max}$ is the maximum ion concentration of ion species "*i*" and is given by $c_{i,\max} = 1/N_A a_i^3$ when assuming simple cubic ion packing. Here, N_A is the Avogadro's number ($N_A = 6.022 \times 10^{23} \text{ mol}^{-1}$). Note that as the ion diameter vanishes, i.e., $a_i = 0$, $c_{i,\max}$ tends to infinity and γ_i approaches 1. It is also interesting to note that eq 4 is a simplified expression of the activity coefficient based on the Boublik–Mansoori–Carnahan– Starling–Leland equation-of-state.^{21,56–58}

By employing the "Langmuir type" activity coefficient given by eq 4, the GMPNP model can be written as

$$\begin{cases} \nabla \cdot (\varepsilon_0 \varepsilon_r \nabla \psi) = -F \sum_{i=1}^N z_i c_i & (5a) \\ \frac{\partial c_i}{\partial t} = \nabla \cdot \left(\frac{D_i F z_i c_i}{R_u T} \nabla \psi + D_i \nabla c_i + \frac{D_i N_A c_i \sum_{i=1}^N a_i^3 \nabla c_i}{1 - N_A \sum_{i=1}^N a_i^3 c_i} \right) & (5b) \end{cases}$$

Note that for vanishing ion diameter $(a_i = 0)$, eqs 3 and 5 reduce to the classical PNP model.⁹ In addition, for binary and symmetric electrolytes, N = 2, $z_1 = -z_2$, $D_1 = D_2$, and $a_1 = a_2$, and eqs 3 and 5 reduce to the MPNP model developed in refs 19 and 21. Note also that the GMPNP model can be also derived by considering the excess chemical potential μ_i^{ex} for each ion species "*i*" and by noting its direct relation to the activity coefficient γ_i given by $\mu_i^{ex} = k_{\rm B}T \ln(\gamma_i)$.^{21,68,70} Compared with previous MPNP models,

Compared with previous MPNP models, $^{3,17-23,47-30,03-07}$ the present generalized MPNP (GMPNP) model, given by eqs 3 to 5, has several attractive features. First, it applies to asymmetric electrolytes and/or multiple ion species. Second, it does not present any additional challenges in the numerical solution procedure compared with the MPNP model for binary symmetric electrolytes. $^{9,17,19-23}$ Moreover, it can be conveniently applied to three-dimensional geometries unlike those expressed as integral-differential equations. $^{45-48}$ Third, it is consistent with the classical or existing models when considering ions as point charges or having identical diameters. Fourth, it can be readily extended by employing other forms of activity coefficient based on available expressions of excess chemical potential μ_i^{ex} such as the Boublik–Mansoori–Carnahan–Starling–Leland equation-of-state. 21,58

3.2. Schematics and Assumptions. In the present study, the double layer structure with multiple Stern layers proposed in refs 36-40 was not adopted because this does not satisfy the overall electroneutrality condition, as discussed previously. Instead, the electric double layer was assumed to consist of (i) a single Stern layer adjacent to the electrode surface and (ii) a diffuse layer beyond. Wang et al.^{9,16} previously showed that the

electrode curvature has negligible effect on the areal integral capacitance for electrode or pore radii larger than 40 nm. Therefore, analysis of planar electrodes is representative of macroporous and mesoporous electrodes with large enough radii of curvature.

Figure 1a shows the half domain used in previous simulations for binary and symmetric electrolytes.⁹ By contrast, Figure 1b shows the schematic of the computational domain used to simulate the electrolyte solution consisting of binary asymmetric electrolytes between two identical planar electrodes A and B. In the present study, simulations with the former and the latter domains were referred to as "half-domain simulations" and "full-domain simulations", respectively. Here, the effective ion diameters of the larger and smaller ion species were denoted by a_1 and a_2 , respectively. The region of electrolyte solution consisted of three layers including (1) the Stern layer of thickness H near each electrode surface located at $x = \pm L$ and (2) the diffuse layer between the Stern layers, i.e., -L + $H \le x \le L - H$. Here, the thickness H was approximated as the effective radius of the largest ion referred to as ion species 1, i.e., $H = a_1/2.$

To make the problem mathematically tractable, the following assumptions were made: (1) the effective ion diameter was assumed to be independent of electrolyte concentration, 19,21,74 (2) the electrolyte dielectric permittivity was constant and equal to that of water. Note that the dielectric permittivity may depend on electric field and temperature. 13,16,75,76 However, it is typically assumed to be constant in scaling analysis, as performed in refs 11, 12, 19–23, and 77. (3) isothermal conditions prevailed throughout the electrode and electrolyte, (4) advection of the electrolyte was assumed to be negligible, (5) the ions could only accumulate at the electrode surface and could not diffuse into the electrode, i.e., there was no ion insertion, and (6) the specific ion adsorption due to nonelectrostatic forces was assumed to be negligible.

3.3. One-Dimensional Formulation. The local electric potential $\psi(x,t)$ in the identical solid electrodes A and B of electrical conductivity σ_s and thickness L_s was governed by the Poisson equation expressed as^{9,78,79}

$$\frac{\partial}{\partial x} \left(\sigma_{s}^{s} \frac{\partial \psi}{\partial x} \right) = 0 \text{ for } -L_{s} - L \leq x < -L \text{ and } L < x \leq L + L_{s}$$
(6)

Moreover, the local electric potential $\psi(x,t)$ and molar ion concentrations $c_i(x,t)$ at time t and location x in the binary asymmetric electrolyte solution were computed by solving the generalized MPNP model with a Stern layer. For planar electrodes, the generalized MPNP model (eqs 5) in the diffuse layer $(-L + H \le x \le L - H)$ can be expressed in its onedimensional form as

$$\begin{cases} \frac{\partial}{\partial x} \left(\varepsilon_0 \varepsilon_r \frac{\partial \psi}{\partial x} \right) = -F \sum_{i=1}^2 z_i c_i \quad (7a) \\ \frac{\partial c_i}{\partial t} = -\frac{\partial N_i}{\partial x} \quad (7b) \end{cases}$$

Here, N_i denotes the mass flux of ion species "i" expressed as

$$N_{i}(x, t) = -\frac{D_{i}Fz_{i}c_{i}}{R_{u}T}\frac{\partial\psi}{\partial x} - D_{i}\frac{\partial c_{i}}{\partial x} - \frac{D_{i}N_{A}c_{i}}{1 - N_{A}\sum_{i=1}^{2}a_{i}^{3}c_{i}}\frac{\partial}{\partial x}(\sum_{i=1}^{2}a_{i}^{3}c_{i})$$

$$(8)$$

Here, the surface potentials at the surface of electrode A ($x = -L - L_s$) and B ($x = L + L_s$) were imposed to be $-\psi_s(t)$ and $+\psi_s(t)$, respectively, where $\psi_s(t)$ is given by eq 1. Moreover, the Stern layers can be accounted for via the boundary conditions relating the potential drop across the Stern layer and the potential gradient at the Stern/diffuse layer interface located at x = (L - H) and x = -(L - H).^{16,19,21} Then, it suffices to simulate only the diffuse layer in the computational domain defined by $-L + H \le x \le L - H$.^{16,19,21} For planar electrodes, the boundary conditions accounting for the Stern layers are given by^{16,19,21}

$$\frac{\partial \psi}{\partial x}(x = L - H, t) = \frac{1}{H}[\psi(x = L, t) - \psi(x = L - H, t)]$$
(9a)

and

$$\frac{\partial \psi}{\partial x}(x = -L + H, t) = \frac{1}{H}[\psi(x = -L, t) - \psi(x = -L + H, t)]$$
(9b)

The electric potential and current density were continuous across the electrode/electrolyte interface located at $x = \pm L$ so that^{9,80}

$$\psi(x = -L^{-}, t) = \psi(x = -L^{+}, t) \text{ and}$$
$$- \sigma_{s} \frac{\partial \psi}{\partial x} (x = -L^{-}, t) = -\varepsilon_{0} \varepsilon_{r} \frac{\partial^{2} \psi}{\partial x \partial t} (x = -L^{+}, t)$$
(10a)

$$\psi(x = L^{-}, t) = \psi(x = L^{+}, t) \quad \text{and}$$
$$- \sigma_{s} \frac{\partial \psi}{\partial x} (x = L^{+}, t) = -\varepsilon_{0} \varepsilon_{r} \frac{\partial^{2} \psi}{\partial x \partial t} (x = L^{-}, t) \quad (10b)$$

Moreover, at the Stern/diffuse layer interface located at $x = \pm (L - H)$, the mass fluxes of ion species vanish since there is no ion insertion in the electrode material (assumption 5) such that

$$N_i(-L+H, t) = 0$$
 and $N_i(L-H, t) = 0$ (11)

The initial conditions in the diffuse layer satisfy the electroneutrality condition and are given by

$$\psi(x, t = 0) = 0, c_1(x, t = 0) = c_{1,\infty} \text{ and}$$

 $c_2(x, t = 0) = -c_1 \sum_{n=1}^{\infty} z_1/z_2$
(12)

where $c_{i,\infty}$ represents the bulk ion concentration of ion species "*i*".

Note that the Ohmic IR drop due to the electrolyte solution is typically the major source of resistance. It is often accounted for via a resistance in an equivalent RC circuit while ignoring the electric double layer structure.^{1,81} By contrast, the present study accounted for the detailed electric double layer structure. Thus, the electric potential drop in the electrolyte solution was rigorously obtained by numerically solving the GMPNP model along with the boundary conditions (eqs 7–12).

3.4. Dimensional Analysis. Equations 6–12 constitute the one-dimensional generalized MPNP model with a Stern layer

for binary asymmetric electrolytes accounting for the electrodes. Based on our previous studies,⁹ the following scaling parameters were introduced:

$$x^* = \frac{x}{\lambda_D}, \ t^* = \frac{tD_1}{\lambda_D^2}, \ \psi^* = \frac{\psi}{R_u T/z_1 F}, \ \text{and} \ c_i^* = \frac{c_i}{c_{1,\infty}}$$
(13)

where $\lambda_{\rm D} = (\varepsilon_0 \varepsilon_{\rm r} R_{\rm u} T / F^2 \sum_{i=1}^2 z_i^2 c_{i,\infty})$ is the Debye length for binary asymmetric electrolytes.⁸² Then, the governing eq 6 in the electrode can be expressed, in dimensionless form, as

$$\frac{\partial}{\partial x^*} \left(\frac{\partial \psi^*}{\partial x^*} \right) = 0 \quad \text{for} \quad -(L_s + L)/\lambda_D \le x < -L/\lambda_D$$

and $L/\lambda_D < x \le (L + L_s)/\lambda_D$ (14)

Similarly, the governing eqs 7 in the electrolyte were transformed into the dimensionless as,

$$\frac{\partial^2 \psi^*}{\partial x^{*2}} = -\frac{c_1^* + z_2^* c_2^*}{1 - z_2^*} \quad (15a)$$
$$\frac{\partial c_i^*}{\partial t^*} = -\frac{\partial N_i^*}{\partial x^*} \quad (15b)$$

for $(-L + a_1/2)/\lambda_D \le x^* \le (L - a_1/2)/\lambda_D$ with the dimensionless ion flux N_i^* given by

$$N_{i}^{*}(x^{*}, t^{*}) = -\frac{D_{i}}{D_{1}} \frac{\partial c_{i}^{*}}{\partial x^{*}} - \frac{D_{i}}{D_{1}} \frac{z_{i}}{z_{1}} c_{i}^{*} \frac{\partial \psi^{*}}{\partial x^{*}} - \frac{D_{i}}{D_{1}} \frac{c_{i}^{*}}{2 - \sum_{i=1}^{2} \nu_{pi} c_{i}^{*}} \frac{\partial}{\partial x^{*}} \sum_{i=1}^{2} \nu_{pi} c_{i}^{*}$$
(16)

where $z_2^* = z_2/z_1$ is the ratio of valencies between smaller and larger ion species, i.e., $z_2^* = -1$ for symmetric electrolytes. Here, the packing parameter for ion species "*i*" is defined as $v_{pi} = 2c_{1\infty}/(1/a_i^3N_A)$. It represents the ratio of the total bulk ion concentration to the maximum ion concentration $1/a_i^3N_A$ assuming a simple cubic packing of ions of diameter a_i .

The dimensionless potential $\psi_s^*(t)$ imposed at the electrode surface in CV measurements is given by

$$\psi_{\max}^* - v^* [t^* - 2(m-1)\tau_{CV}^*]$$
(17a)
for $2(m-1)\tau_{TV}^* \le t^* \le (2m-1)\tau_{TV}$

$$\psi_{s}^{*}(t^{*}) = \begin{cases} v_{\text{min}}^{*} t^{*} + v^{*}[t^{*} - (2m - 1)\tau_{\text{CV}}^{*}] \\ \psi_{\text{min}}^{*} t^{*} + v^{*}[t^{*} - (2m - 1)\tau_{\text{CV}}^{*}] \\ \text{for } (2m - 1)\tau_{\text{CV}}^{*} \le t^{*} \le 2m\tau_{\text{CV}}^{*} \end{cases}$$
(17b)

where $\tau_{CV}^* = (\psi_{max}^* - \psi_{min}^*)/v^*$ represents the dimensionless half cycle period and $v^* = (\lambda_D^2/D_1)/[(R_uT/z_1F)/v]$ is the dimensionless scan rate. It can be interpreted as the ratio of the ion diffusion time scale (λ_D^2/D_1) and the characteristic time for reaching the thermal potential R_uT/z_1F at scan rate v. Moreover, $\psi_{max}^* = \psi_{max}/(R_uT/z_1F)$ and $\psi_{min}^* = \psi_{min}/(R_uT/z_1F)$ are the maximum and minimum surface potentials, respectively, scaled by the thermal potential. They can be also interpreted as the ratio of characteristic times to reach ψ_{max} or ψ_{min} and the characteristic time for reaching the thermal potential at scan rate v.

Moreover, the boundary conditions [eqs 9 and 11] at the Stern/diffuse layer interface located at $x^* = \pm (L - a_1/2)/\lambda_D$ can be written in dimensionless form as

$$\frac{2}{a_1^*} \frac{\partial \psi^*}{\partial x^*} (x^* = L^* - a_1^*/2, t^*)$$

= $\psi^* (x^* = L^*, t^*) - \psi^* (x^* = L^* - a_1^*/2, t^*)$
(18a)

$$-\frac{1}{a_1^*}\frac{1}{\partial x^*}(x^* = -L^* + a_1^*/2, t^*)$$

$$= -\psi^*(x^* = -L^*, t^*) - \psi^*(x^* = -L^* + a_1^*/2, t^*)$$
(18b)
$$N_i^*(L^* - a_1^*/2, t^*) = N_i^*(-L^* + a_1^*/2, t^*) = 0$$
(18c)

where $L^* = L/\lambda_D$ and $a_1^* = a_1/\lambda_D$ are respectively the half interelectrode distance and effective ion diameter scaled by the Debye length representing the thickness of the electric double layer. Similarly, the boundary conditions (eqs 10) at the electrode/electrolyte interface located at $x^* = \pm L/\lambda_D$ became, in dimensionless form,

$$\psi^*(x^* = \pm L^{\pm}/\lambda_D) = \psi^*(x^* = \pm L^{\mp}/\lambda_D)$$
 (19a)

and

$$\frac{\sigma_{s}^{*}}{\psi_{\max}^{*} - \psi_{\min}^{*}} \frac{L_{s}^{*}}{L^{*}} \frac{\partial \psi^{*}}{\partial x^{*}} (x^{*} = \pm L^{\pm} / \lambda_{D})$$

$$= \frac{\partial^{2} \psi^{*}}{\partial x^{*} \partial t^{*}} (x^{*} = \pm L^{\mp} / \lambda_{D}) \tag{19b}$$

where $L_s^* = L_s/\lambda_D$ is the electrode thickness scaled by the Debye length. Note that $\sigma_s^* = [\sigma_s(\psi_{max} - \psi_{min})/L_s(Fz_1c_{1\infty}D_1/L)]$ represents the ratio of the characteristic current density in the electrode to that in the electrolyte. It can be also interpreted as the ratio of time scales for charge transport in the electrolyte and in the electrode.

Similarly, the dimensionless initial conditions for ψ^* and c_i^* in the diffuse layer, for $-L^* + a_1^*/2 \le x^* \le L^* - a_1^*/2$, simplify as

$$\psi^*(x^*, t^* = 0) = 0, \quad c_1^*(x^*, t^* = 0) = 1, \quad \text{and} \\
c_2^*(x^*, t^* = 0) = -1/z_2^*$$
(20)

Considering the dimensionless governing equations and associated boundary and initial conditions, eleven key dimensionless similarity parameters can be identified as

$$\nu^{*} = \frac{\lambda_{\rm D}^{2}/D_{1}}{(R_{\rm u}T/z_{1}F)/\nu}, \quad \psi_{\rm max}^{*} = \frac{\psi_{\rm max}}{R_{\rm u}T/z_{1}F}, \\
\psi_{\rm min}^{*} = \frac{\psi_{\rm min}}{R_{\rm u}T/z_{1}F}, \quad L^{*} = \frac{L}{\lambda_{\rm D}}, \quad a_{1}^{*} = \frac{a_{1}}{\lambda_{\rm D}}, \\
\nu_{\rm p1} = 2a_{1}^{3}N_{\rm A}c_{1\infty}, \quad \nu_{\rm p2} = 2a_{2}^{3}N_{\rm A}c_{1\infty}, \quad D_{2}^{*} = \frac{D_{2}}{D_{1}}, \\
z_{2}^{*} = \frac{z_{2}}{z_{1}}, \quad \sigma_{\rm s}^{*} = \frac{\sigma_{\rm s}(\psi_{\rm max} - \psi_{\rm min})/L_{\rm s}}{Fz_{1}c_{1\infty}D_{1}/L}, \quad \text{and} \quad L^{*} = \frac{L_{\rm s}}{\lambda_{\rm D}}$$
(21)

where v_{p1} represents the packing parameter due to finite ion size of ion species "1". Note that v^* , ψ^*_{max} , ψ^*_{min} , L^* , a_1^* , and v_{p1} were identical to or direct functions of those identified in ref 9 for the CV simulations of electric double layer capacitors with binary symmetric electrolytes. When considering binary asymmetric electrolytes, three additional dimensionless numbers appear, namely, v_{p2} , D_2^* , and z_2^* . The dimensionless numbers σ_s^* and L_s^* account for the charge transport in the electrode.

3.5. Constitutive Relations. In order to solve eqs 7-12 or eqs 15–20, the electrolyte properties ε_r , a_i , z_i , D_i , $c_{1\infty}$ along with the temperature T, and the surface potential $\psi_s(t)$ are needed. The present study focuses on binary electrolytes at room temperature T = 298 K with different ion diameter, diffusion coefficient, and/or valency. The electrolyte relative permittivity was taken as that of water $\varepsilon_r = 78.5^{24}$ while the effective ion diameter a_i ranged from 0.60 to 1.0 nm typical of solvated ion diameters.⁷⁴ The valencies $(z_1: z_2)$ corresponded also to realistic conditions including 1: -1, 1: -2, 2: -2, or 1: -3. The ion diffusion coefficients D_i varied from $1.957 \times 10^{-9} \text{ m}^2/\text{s}$ to 5.273×10^{-9} m²/s representative of aqueous and organic electrolytes.²⁴ The initial and bulk ion concentrations was $c_{1,\infty} = 1.0 \text{ mol/L}$ and $c_2 = -c_{1,\infty}z_1/z_2$ satisfying the overall electroneutrality condition. Moreover, the maximum and minimum surface electric potentials were $\psi_{max} = 0.5$ V and ψ_{\min} = -0.5 V, respectively. The scan rate in actual CV measurements for electrical energy storage devices ranges typically from 10^{-3} to 200 V/s.⁴⁻⁸ Here, the scan rate ν varied over a wider range from 10^{-2} to 10^{8} V/s. This was due to two main reasons. First, small electrode thickness (0–100 nm) was considered along with realistic values (>1 μ m) to validate the scaling analysis. The capacitance starts to decrease at very large scan rate for such small electrode thickness.⁹ Second, asymptotic behaviors of electric double layers were explored at very large scan rates. Our previous study⁹ established that electric double layers behave as a resistor under such conditions. Finally, the electrode electrical conductivity was chosen to be 10^{-5} to 10^2 S/m, typical of carbon materials.^{83,84}

3.6. Method of Solution. The governing eqs 7 and 8 were solved along with the boundary and initial conditions given by eqs 9–12 using the commercial finite element solver COMSOL 4.2. CV measurements were simulated by numerically imposing the periodic surface electric potential given by eq 1.

Simulations of CV measurements were performed for at least three cycles. The numerical convergence criterion was defined such that the maximum relative difference in the predicted capacitive current density $j_{\rm C}$ was less than 1% when (i) reducing the mesh size by a factor of 2 and (ii) dividing the time step by two. The mesh size was the smallest at the electrode surfaces due to the large potential gradient and then gradually increased. Converged solutions were achieved by imposing a time step of $\Delta t \approx t_0/800 = (\psi_{\rm max} - \psi_{\rm min})/800\nu$ with the mesh size $\Delta x/L =$ 5×10^{-14} at the Stern/diffuse layer interface with a growth rate of 1.3 up to $\Delta x/L = 1/250$ in the rest of the domain. Based on these convergence criteria, the total number of finite elements was less than 1910 for all cases simulated in the present study.

3.7. Data Processing. The capacitive current density j_C from CV simulations was computed based on its definition as^{9,85-88}

$$j_{C}(t) = -\varepsilon_{0}\varepsilon_{r}\frac{\partial^{2}\psi}{\partial x\partial t}\Big|_{x_{L}or-x_{L}} \text{ at } x_{L} = L - H \text{ or}$$
$$-x_{L} = -(L - H) \tag{22}$$

The corresponding dimensionless capacitive current density $j_{\rm C}^*$ at $x_L^* = L^* - a_1^*/2$ and $-x_L^* = -L^* + a_1^*/2$ is expressed as

$$j_{\rm C}^{*}(t^{*}) = \frac{j_{\rm C}(t)}{F z_1 D_1 c_{1,\infty} / \lambda_D} = -\sum_{i=1}^2 z_i^{*2} c_{i,\infty}^{*} \frac{\partial^2 \psi^{*}}{\partial x^{*} \partial t^{*}} \bigg|_{x_L^{*} \text{or} - x_L^{*}}$$
(23)

In order to reproduce typical CV measurements, the current densities $j_{\rm C}(t)$ and $j_{\rm C}^*(t^*)$ were plotted as functions of $\psi_s(t)$ and $\psi_s^*(t^*)$, respectively.

3.8. Validation. The numerical tool was validated based on existing solutions reported in the literature. The transient ion concentration and electric potential profiles were predicted by solving the PNP and MPNP models for binary and symmetric electrolytes (N = 2, $z_1 = -z_2 = z$, and $a_1 = a_2$) with constant surface electric potential. The results were successfully compared with the reported numerical solutions for $c_i(x,t)$ and $\psi(x,t)$ for a wide range of packing parameter v_p and dimensionless surface potential ψ_s^* .¹⁹

4. RESULTS AND DISCUSSION

Results in the Supporting Information (Figures S2 and S3) demonstrate that half-domain CV simulations should only be used for symmetric electrolytes while the full domain must be simulated for asymmetric electrolytes. Consequently, all the following CV simulations were performed for the entire domain consisting of electrolyte solution between two identical planar electrodes.

4.1. Asymmetric versus Symmetric Electrolytes. 4.1.1. Effect of Asymmetric Ion Diameter. Figure 2 shows



Figure 2. Predicted $j_{\rm C}$ versus $\psi_{\rm s}$ curves from CV simulations for three cases with different ion diameters, namely, (i) $a_1 = a_2 = 0.60$ nm, (ii) $a_1 = 0.66$ and $a_2 = 0.60$ nm, and (iii) $a_1 = a_2 = 0.66$ nm. Results were obtained by solving the GMPNP model with a Stern layer (eqs 6–12) without accounting for the potential drop across the electrodes corresponding to $\sigma_s \rightarrow \infty$ S/m or $L_s = 0$ m. Other parameters were $c_{1,\infty} = 1 \text{ mol/L}, v = 10^4 \text{ V/s}, L = 200 \ \mu\text{m}, \psi_{\text{max}} = \psi_{\text{min}} = 0.5 \text{ V}, T = 298 \text{ K}, \text{ and } \varepsilon_r = 78.5.$

CV curves predicted for three cases with different ion diameters, namely (i) $a_1 = a_2 = 0.60$ nm, (ii) $a_1 = 0.66$ nm and $a_2 = 0.60$ nm, and (iii) $a_1 = a_2 = 0.66$ nm. The ion valencies and diffusion coefficients were $z_1 = -z_2 = 1$ and $D_1 = D_2 = 1.957 \times 10^{-9}$ m²/s, respectively. Other parameters were $c_{1,\infty} = 1$ mol/L, $v = 10^4$ V/s, $L = 200 \ \mu$ m, $\psi_{max} = \psi_{min} = 0.5$ V, T = 298 K, and $\varepsilon_r = 78.5$. Results were obtained by solving the GMPNP model with a Stern layer (eqs 6–12) without accounting for the potential drop across the electrodes corresponding to $\sigma_s \rightarrow \infty$ S/m or $L_s = 0$ m. Figure 2 demonstrates that the current density j_C for asymmetric electrolyte with $a_1 = 0.66$ nm and $a_2 = 0.60$ nm lay between those obtained

for symmetric electrolytes with ion diameter *a* equal to 0.66 and 0.60 nm. The relative difference in j_C between asymmetric and symmetric electrolytes was about 9%. Figure 2 also indicates that the predicted current density j_C increased with decreasing ion diameter. This can be attributed to the fact that smaller ions have larger maximum ion concentrations $c_{i,\text{max}}$ and thus feature a larger gradient in electric potential near the electrode surface.²¹ This, in turn, led to a larger capacitive current density according to eq 22. Overall, these results demonstrate that the unequal ion size needs to be accounted for in order to accurately predict the current density for asymmetric electrolytes.

4.1.2. Effect of Asymmetric Valency. Figure 3 shows the CV curves predicted for electrolytes with different valencies, namely



Figure 3. Predicted j_c versus ψ_s curves from CV simulations for three cases with different valencies, namely, (i) $z_1 = -z_2 = 2$, (ii) $z_1 = 1$ and $z_2 = -2$, and (iii) $z_1 = -z_2 = 1$. The model and other parameters were identical to those used to generate the results shown in Figure 2.

(i) $z_1 = -z_2 = 1$, (ii) $z_1 = 1$ and $z_2 = -2$, and (iii) $z_1 = -z_2 = 2$. Here, the ion diameters and diffusion coefficients were identical such that $a_1 = a_2 = 0.60$ nm, $D_1 = D_2 = 1.957 \times 10^{-9}$ m²/s, and $L_s = 0$ m. It is evident that the predicted current density j_C for asymmetric valency $z_1 = 1$ and $z_2 = -2$ lay between those obtained for symmetric valency with $z_1 = -z_2 = 1$ and $z_1 = -z_2 = 2$. The relative difference in current density j_C between asymmetric and symmetric electrolytes was about 9%. Moreover, j_C increased with increasing valency $|z_i|$. This can be attributed to the fact that increasing the valency $|z_i|$ led to increasing the amount of charges accumulated near the electrode surface. This, in turn, led to a larger local electric field near the electrode surface and thus larger current density.

4.1.3. Effect of Asymmetric Diffusion Coefficient. Figures 4 show $j_{\rm C}$ versus $\psi_{\rm s}$ predicted at (a) low scan rate $\nu = 10^2$ V/s and (b) high scan rate $v = 10^5$ V/s for three cases with different ion diffusion coefficients, namely (i) $D_1 = D_2 = 2.69D_0$, (ii) $D_1 = D_0$ and $D_2 = 2.69 D_0$, and (iii) $D_1 = D_2 = D_0$ with $D_0 = 1.957 \times$ 10^{-9} m²/s. The ion diameter and valency were identical, namely, $a_1 = a_2 = 0.60$ nm and $z_1 = -z_2 = 1$, while the electrode thickness was zero, i.e., $L_s = 0$ m. Figure 4a demonstrates that, at low scan rate $v = 10^2$ V/s, the predicted CV curves overlapped for all three cases despite differences in diffusion coefficients. Moreover, the CV curves were symmetric about the $j_C = 0$ axis. Note that similar phenomena were also observed in CV simulations for binary and symmetric electrolytes.9 This can be attributed to the fact that ion transport is diffusion-independent at low scan rates⁹ and is controlled by the electric field. On the other hand, Figure 4b



Figure 4. Predicted $j_{\rm C}$ versus $\psi_{\rm s}$ curves from CV simulations for (a) v = 102 V/s and (b) $v = 10^5$ V/s. Three cases with different ion diffusion coefficients were considered, namely, (i) $D_1 = D_2 = 2.69D_0$, (ii) $D_1 = D_0$ and $D_2 = 2.69D_0$, and (iii) $D_1 = D_2 = D_0$ along with $D_0 = 1.957 \times 10^{-9}$ m²/s. The model and other parameters were identical to those used to generate the results shown in Figure 2.

demonstrates that the predicted CV curves became distorted at large scan rate $v = 10^5$ V/s. Here, the predicted current density j_C and thus the capacitance increased with increasing ion diffusion coefficient D_1 or D_2 . Indeed, larger diffusion coefficients enable ions to better follow the rapid variations in electric potential.⁹ These results demonstrate that asymmetric ion diffusion coefficients must be accounted for in CV simulations at large scan rates but have no effect on CV curves at low scan rates.

4.2. Dimensional Analysis. Table 1 summarizes the different values of v, L, T, ψ_{max} , ψ_{min} , a_i , D_i , z_i , and $c_{i\infty}$ for four different cases of binary asymmetric electrolytes considered. Parameters used in Case 1 corresponded to aqueous asymmetric electrolyte KOH.^{9,24,74} Note that the dimensionless numbers for all four cases were identical, namely, $v^* = 1.8 \times 10^{-5}$, $\psi^*_{max} =$ $-\psi_{\min}^* = 19.5, L^* = 3.29 \times 10^5, a_1^* = 2.17, v_{p1} = 0.346, v_{p2} = 0.26,$ $D_2^* = 2.5, z_2^* = -1, \sigma_s^* \to \infty$, and $L_s^* = 0$. Figures 5a shows the predicted $j_{\rm C}$ versus $\psi_{\rm s}$ curves obtained for these four cases. Results were obtained by numerically solving the generalized MPNP model with a Stern layer (eqs 7-12). Figure 5a indicates that the CV curves were significantly different in these four cases. However, Figure 5b shows that the same data plotted in terms of dimensionless current density $j_{\rm C}^*$ versus dimensionless surface potential ψ_s^* collapsed on a single CV curve. Note that such self-similar behaviors were also observed for cases with $z_2^* = -2$ and $z_2^* = -3$. Overall, these results illustrated that the governing equations and the boundary and initial conditions were properly scaled by parameters defined in

Ta	ab.	le	1.	Parameters	Used	in	CV	Simulations	Reported	in	Figure	5"	
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	$\nu (V/s)$	$L(\mu m)$	T(K)	$\psi_{\rm max}$ = $-\psi_{\rm min}$ (V)	\mathcal{E}_{r}	$a_1 (nm)$	$a_2 (nm)$	$D_1 (m^2/s)$	$D_2 (m^2/s)$	z_1	z_2	$c_{1\infty} \; ({\rm mol/L})$
Case 1	10 ⁴	100	298	0.5	78.5	0.66	0.60	2×10^{-9}	5×10^{-9}	1	-1	1
Case 2	2×10^4	50	298	0.5	157	0.33	0.30	1×10^{-9}	2.5×10^{-9}	1	-1	8
Case 3	1.33×10^{4}	75	298	0.5	104.7	0.495	0.45	1.5×10^{-9}	3.75×10^{-9}	1	-1	2.37
Case 4	1.33×10^{4}	75	89.4	0.15	348.9	0.495	0.45	5×10^{-8}	1.25×10^{-9}	1	-1	2.37
Case 4	1.33×10^{4}	75	89.4	0.15	348.9	0.495	0.45	5×10^{-8}	1.25×10^{-9}	1	-1	2.37

^{*a*}In these four cases, the dimensionless numbers were identical and equal to $v^* = 1.8 \times 10^{-5}$, $\psi^*_{max} = -\psi^*_{min} = 19.5$, $L^* = 3.29 \times 10^5$, $a_1^* = 2.17$, $\nu_{p1} = 0.346$, $\nu_{p2} = 0.26$, $D_2^* = 2.5$, $z_2^* = -1$, $\sigma_s^* \to \infty$, and $L_s^* = 0$.



Figure 5. Predicted (a) $j_{\rm C}$ versus ψ_s curves and (b) $j_{\rm C}^*$ versus ψ_s^* curves from CV simulations for four cases with parameters given in Table 1. Results were obtained by numerically solving the generalized MPNP model with a Stern layer (eqs 7–12) for $v^* = 1.8 \times 10^{-5}$, $\psi_{\rm max}^* = -\psi_{\rm min}^* = 19.5$, $L^* = 3.29 \times 10^5$, $a_1^* = 2.17$, $v_{\rm p1} = 0.346$, $v_{\rm p2} = 0.26$, $D_2^* = 2.5$, $z_2^* = -1$, $\sigma_s^* \to \infty$, and $L_s^* = 0$.

eqs 13. More importantly, they show that the electric double layer dynamics for binary asymmetric electrolytes near planar electrodes in CV measurements were governed by 11 dimensionless similarity parameters, namely, v^* , ψ^*_{max} , ψ^*_{min} , L^* , a_1^* , v_{p1} , v_{p2} , D_2^* , z_2^* , σ_s^* , and L_s^* given by eq 21.

Moreover, a dimensionless areal integral capacitance can be defined as

$$C_{\rm s}^{*} = \frac{C_{\rm s}}{z_{\rm l}eN_{\rm A}D_{\rm l}c_{\rm l,\infty}/\lambda_{\rm D}v} = \frac{1}{\psi_{\rm max}^{*} - \psi_{\rm min}^{*}} \oint \frac{j_{\rm C}^{*}}{2v^{*}} \, \mathrm{d}\psi_{\rm s}^{*}$$
(24)

where C_s is defined in eq 1. Graphically, C_s^* corresponds to the area enclosed by the j_C^* versus ψ_s^* curve. Figure 5b demonstrates that C_s^* depends only on the eleven dimensionless numbers so that $C_s^* = f(v^*, \psi_{\max}^*, \psi_{\min}^*, L^*, a_1^*, v_{p1}, v_{p2}, D_2^*, z_2^*, \sigma_s^*, L_s^*)$. This relation can be used to formulate design rules for



Figure 6. Predicted j_C^* versus ψ_s^* curves from CV simulations for three different values of z_2^* , namely, $z_2^* = -1$, -2, and -3. The model and other dimensionless numbers were identical to those used to generate the results shown in Figure 5.



Figure 7. Predicted (a) capacitance C_s as a function of scan rate v and (b) ratio $C_s/C_{s,0}$ as a function of $2v^*L^*/[(1 + D_2^*)(\psi_{max}^* - \psi_{min}^*)]$ obtained from CV simulations for cases 1 to 17 without accounting for the potential drop across the electrodes (i.e., $\sigma_s^* \to \infty$ or $L_s^* = 0$) with dimensionless parameters L*, z_2^* , $\psi_{max}^* = -\psi_{min}^*$, D_2^* , a_1^* , v_{p1} , and v_{p2} summarized in Table 2.

Table 2. Dimensionless Parameters for 29 Cases of CV Simulations Reported in Figures 7 and 8 along with the Respective Values of Maximum Capacitance $C_{s,0}$

	L^*	z_2^*	$\psi^*_{\max} = -\psi^*_{\min}$	D_2^*	a_1^*	$ u_{\mathrm{p1}}$	$ u_{\mathrm{p2}}$	$\sigma^*_{ m s}$	$L_{\rm s}^*$	$C_{s,0}$ ($\mu F/\mathrm{cm}^2$)
Case 1	32900	-3	19.5	1	2.17	0.346	0.346	00	0	160.1
Case 2	329000	-3	19.5	1	2.17	0.346	0.346	00	0	160.1
Case 3	32900	-2	19.5	1	2.17	0.346	0.346	00	0	127.1
Case 4	329000	-2	19.5	1	2.17	0.346	0.346	00	0	127.1
Case 5	32900	-1	19.5	1	2.17	0.346	0.346	00	0	87.5
Case 6	329000	-1	19.5	1	2.17	0.346	0.346	00	0	87.5
Case 7	329000	-1	0.195	1	2.17	0.346	0.346	00	0	109.6
Case 8	329000	-1	1.95	1	2.17	0.346	0.346	00	0	109.5
Case 9	329000	-1	9.75	1	2.17	0.346	0.346	00	0	102.2
Case 10	329000	-1	14.625	1	2.17	0.346	0.346	00	0	94.44
Case 11	329000	-1	25.35	1	2.17	0.346	0.346	00	0	87.77
Case 12	329000	-1	19.5	0.01	2.17	0.346	0.346	00	0	87.5
Case 13	329000	-1	19.5	0.1	2.17	0.346	0.346	∞	0	87.5
Case 14	329000	-1	19.5	10	2.17	0.346	0.346	00	0	87.5
Case 15	329000	-1	19.5	100	2.17	0.346	0.346	00	0	87.5
Case 16	329000	-1	19.5	1	3.06	0.97	0.26	00	0	65.6
Case 17	329000	-1	19.5	1	1.97	0.26	0.26	∞	0	98.5
Case 18	263.1	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-7}	329	87.5
Case 19	263.1	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-4}	329	87.5
Case 20	263.1	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-1}	329	87.5
Case 21	263.1	-1	19.5	1	2.17	0.346	0.346	∞	329	87.5
Case 22	32900	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-4}	0	87.5
Case 23	32900	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-4}	329	87.5
Case 24	32900	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-4}	3290	87.5
Case 25	32900	-1	19.5	1	2.17	0.346	0.346	1.61×10^{-4}	98400	87.5
Case 26	16400	-3	19.5	100	2.17	0.346	0.346	1.61×10^{-4}	233000	101.4
Case 27	32900	-2	19.5	10	2.17	0.346	0.346	1.61×10^{-4}	98400	97.0
Case 28	403000	-2	19.5	1	2.17	0.346	0.346	0.0566	121000	97.0
Case 29	403000	-2	19.5	10	2.17	0.346	0.346	0.0566	121000	97.0

EDLCs with asymmetric electrolytes. However, finding this multidimensional function falls beyond the scope of this study.

Finally, Figure 6 shows the predicted $j_{\mathbb{C}}^*$ versus ψ_s^* curves for three cases with $z_2^* = -1$, -2, and -3, respectively. The model and the other ten dimensionless numbers were identical to those used to generate the results shown in Figure 5. It is evident that $j_{\mathbb{C}}^*$ and therefore C_s^* increased as z_2^* decreased (i.e., increasing $|z_2^*|$) due to the increase in the amount of charges accumulated at the electrode surface which induced a larger electric current.

4.3. Capacitance versus Scan Rate. Figure 7a shows the double layer areal integral capacitance Cs predicted from CV simulations and estimated using eq 1 as a function of scan rate vranging from 10^{-2} to 10^7 V/s for 17 cases of binary asymmetric electrolytes without accounting for the potential drop across the electrodes. This corresponds to cases with infinitely large electrode electrical conductivity ($\sigma_s \rightarrow \infty$ S/m) or zero electrode thickness ($L_s \rightarrow 0$ m). Table 2 summarizes the values of the 10 dimensionless parameters L^* , z_2^* , $\psi_{max}^* = -\psi_{min}^*$, D_2^* , a_1^* , v_{p1} , v_{p2} , σ_s^* , and L_s^* along with the maximum capacitances $C_{s,0}$ corresponding to the plateau observed in C_s versus v at low scan rates. Note that $C_{s,0}$ depends on a variety of parameters including ψ_s , a_1 , a_2 , z_1 , z_2 , and $c_{1\infty}$. However, it falls beyond the scope of this manuscript to find an analytical expression relating these parameters for asymmetric electrolytes. A remarkably broad range of values were considered for each dimensionless number. It is evident that these C_s versus ν curves as well as $C_{s,0}$ were significantly different from one another. Figure 7b shows the same data as those shown in Figure 7a but plotted in terms

of $C_{\rm s}/C_{\rm s,0}$ as a function of $2\nu^*L^*/[(1 + D_2^*)](\psi_{\rm max}^* - \psi_{\rm min}^*)$. It is interesting to note that all the curves collapsed on a single line, irrespective of the different values of L^* , z_2^* , $\psi_{\rm max}^* = -\psi_{\rm min}^*$, D_2^* , a_1^* , $v_{\rm p1}$, and $v_{\rm p2}$. The Supporting Information presents the effects of each parameter separately. To the best of our knowledge, the present study is the first to identify this selfsimilar behavior of electric double layer integral capacitance in CV measurements with binary asymmetric electrolytes. Fitting the dimensionless data shown in Figure 7b yields the following correlation with a coefficient of determination equal to 0.999

$$\frac{C_{\rm s}}{C_{\rm s,0}} = \frac{1}{1 + \left[\frac{2\upsilon^* L^* / (1 + D_2^*)(\psi_{\rm max}^* - \psi_{\rm min}^*)}{1.22}\right]^{1.44}}$$
(25)

The dimensionless abscissa in Figure 7b can be interpreted as the ratio of two time scales,

$$\frac{2\nu^*L^*}{(1+D_2^*)(\psi_{\max}^*-\psi_{\min}^*)} = \frac{2\lambda_D L/(D_1+D_2)}{(\psi_{\max}-\psi_{\min})/\nu} = \frac{\tau_{\rm RC}}{\tau_{\rm CV}}$$
(26)

where $\tau_{\rm RC}$ is the "RC time scale" for binary asymmetric electrolytes corresponding to the characteristic time of ions' electrodiffusion⁷⁷ and $\tau_{\rm CV}$ is the half cycle period of CV measurements. They are expressed as

$$\tau_{\rm RC} = \sqrt{\tau_{\rm L} \tau_{\rm D}} = \frac{\lambda_{\rm D} L}{(D_1 + D_2)/2} \quad \text{and} \quad \tau_{\rm CV} = \frac{\psi_{\rm max} - \psi_{\rm min}}{v}$$
(27)

Here, $\tau_L = 2L^2/(D_1 + D_2)$ is the time scale for ion diffusion in binary asymmetric electrolytes and $\tau_D = 2\lambda_D^2/(D_1 + D_2)$ has been termed as the "charge relaxation time scale".⁷⁷ Note that $\tau_{\rm RC}$ reduces to the corresponding "RC time scale" of binary symmetric electrolytes when $D_2^* = 1$ as considered in refs 22, 23, and 77. Figure 7b indicates that two regimes can be clearly identified: (i) $2\nu^*L^*/[(D_1 + D_2^*)(\psi_{\rm max}^* - \psi_{\rm min}^*)] \ll 1$ or $\tau_{\rm RC} \ll \tau_{\rm CV}$ corresponds to the quasi-equilibrium or ion diffusion-independent regime and (ii) $2\nu^*L^*/[(D_1+D_2^*)-(\psi_{\rm max}^* - \psi_{\rm min}^*)] \ll 1$ or $\tau_{\rm RC} \ll \tau_{\rm CV}$, corresponds to ion diffusionlimited regime.

4.4. Effect of the Electrode. The above simulations ignored the potential drop across the electrodes. Figure 8a



Figure 8. Predicted (a) capacitance C_s as a function of scan rate v and (b) ratio $C_s/C_{s,0}$ as a function of $T_{\rm RC}/T_{\rm CV}$ (1 + 80/ σ_s^*) obtained from CV simulations for cases 18 to 29 with dimensionless parameters L^* , z_2^* , $\psi_{\rm max}^* = -\psi_{\rm min}^*$, D_2^* , a_1^* , $v_{\rm p1}$, $v_{\rm p2}$, σ_s^* , and L_s^* summarized in Table 2.

shows the double-layer areal integral capacitance C_s predicted from CV simulations as a function of scan rate ν ranging from 10^{-2} to 10^8 V/s for 12 cases accounting for charge transport in the electrodes. Table 2 summarizes the values of the eleven dimensionless parameters L^* , z_2^* , $\psi_{max}^* = -\psi_{min}^*$, D_2^* , a_1^* , ν_{p1} , ν_{p2} , σ_s^* , and L_s^* along with the maximum capacitances $C_{s,0}$ for cases 18 to 29. It is evident that the curves C_s versus ν were significantly different from one another due to the broad range of parameters considered. Figure 8b shows the same data as those shown in Figure 8a but plotted in terms of $C_s/C_{s,0}$ as a function of $\tau_{RC}/\tau_{CV}(1 + 80/\sigma_s^*)$. The fitted curve given by eq 25 for cases ignoring the potential drop across the electrodes ($\sigma_s^* \rightarrow \infty$ or $L_s^* \rightarrow 0$) was also shown in Figure 8b for comparison purposes. It is interesting to note that all the curves collapsed on a single line, irrespective of the different values of L^* , z_2^* , $\psi_{\max}^* = -\psi_{\min}^*$, D_2^* , a_1^* , v_{p1} , v_{p2} , σ_s^* , and L_s^* .

The dimensionless abscissa in Figure 7b can be interpreted as

$$\frac{\tau_{\rm RC}}{\tau_{\rm CV}} \left(1 + \frac{80}{\sigma_{\rm s}^*} \right) = \frac{\tau_{\rm RC}}{\tau_{\rm CV}} \left(1 + 80\frac{\tau_{\rm s}}{\tau_{\rm d}} \right) \tag{28}$$

where $\sigma_s^* = \tau_d/\tau_s$ represents the ratio of characteristic charge transport time scale in the electrolyte τ_d to that in the electrode τ_s as discussed previously. Note that when σ_s^* is very large (e.g., $\sigma_s^* \gg 80$), the charge transport in the electrode is much faster than that in the electrolyte. Then, it suffices to simulate the electrolyte in CV simulations.

5. CONCLUSIONS

This paper developed a MPNP model for simulating electric double layer dynamics. This model was derived from first principles based on excess chemical potential and Langmuir activity coefficient accounting simultaneously for (1) asymmetric electrolytes with (2) multiple ion species of (3) finite ion size, and (4) Stern and diffuse layers. This study established that asymmetric ion diameters and valencies must be accounted for in CV simulations with asymmetric electrolytes for all scan rates. By contrast, asymmetric ion diffusion coefficient affected the CV curves only at large scan rates.

Dimensional analysis of the governing equations was also performed for CV measurements with planar electrodes. Eleven dimensionless numbers given by eq 21 were identified to govern the CV measurements of electric double layer in binary asymmetric electrolytes between two identical planar electrodes of finite thickness. For the first time, a self-similar behavior was identified for the electric double layer integral capacitance estimated from CV measurements with binary asymmetric electrolytes and planar electrodes. The physical interpretations were also provided. This model provides a theoretical framework to investigate more complex situations with asymmetric electrolytes and/or multiple ion species such as redox reactions in pseudocapacitors and the interplay of Faradaic and capacitive currents encountered in fast-scan cyclic voltammetry.

ASSOCIATED CONTENT

S Supporting Information

Results of full domain and half domain simulations as well as the scaling analysis for interelectrode distance, potential window, asymmetric diffusion coefficients, and ion diameter. This material is available free of charge via the Internet at http://pubs.acs.org.

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Notes

The authors declare no competing financial interest.

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